

Simulation-based and statistical tools for uncertainty quantification in a digital twin of a steam generator

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2. Clogging physical and numerical models
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Clogging of steam generators (SGs)

- ▶ Clogging of SGs is a complex multiphysics phenomenon that occurs following long operational periods in pressurized-water reactors (PWR) of the French nuclear fleet → undermines performance & weakens the structures → *may require chemical cleanings*

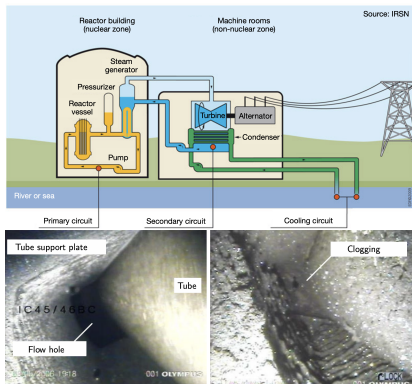


Figure: PWR scheme, and example of video examination during an PWR outage (© IRSN, EDF)

Clogging of SGs

- ▶ No state-of-the-art model allowing for ground insights on diagnosis and prognosis of clogging rate τ_c → very hard to model & challenging to create reproducible lab experiment for model validation + not a lot of literature [Srikantiah and Chappidi, 2000; Prusek et al., 2013; Girard, 2014; Yang et al., 2017]
- ▶ Available scarce video field data as well as indirect measurements → allow to construct data-driven regression algorithms [Pincioli et al., 2021] ≈ not enough data to have robust predictive models
- ▶ Another tool is the physical clogging model developed by [Prusek et al., 2013] → subsequent numerical model THYC-Puffer-DEPO [Feng et al., 2023] ≈ lack of enough trustworthy field data for precise validation
- ▶ Necessary decision-making on chemical cleaning planning under uncertainty → *how to make use of the available knowledge and models for achieving reliable predictions?*

Towards digital twins (DTs) in nuclear industry

- ▶ Growing interest of creating digital twins for nuclear industry → many industrial challenges to address

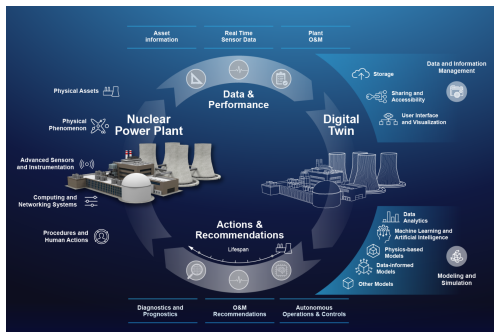


Figure: DT methodologies for nuclear reactors [Vaibhav and al., 2023]

- ▶ Stepping stone towards the elaboration of DT for SGs at EDF → more details in E. Remy's talk - MS018D on Friday morning

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The long-term clogging model

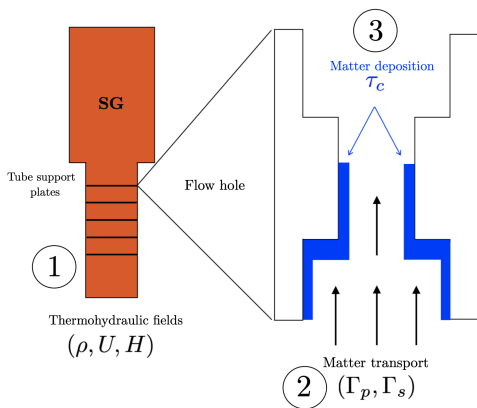


Figure: Clogging physical model

- ▶ Clogging results from two main mechanisms \rightarrow *vena contracta* & *flashing* [Prusek et al., 2013]
- ▶ Long-term clogging model [Feng et al., 2023] \rightarrow must change stationary thermohydraulics + compute chemical conditioning

The numerical model: THYC-Puffer-DEPO

- ▶ THYC-Puffer-DEPO (TPD) is the chaining of 3 codes → allows to simulate SG clogging on entire lifespan of the asset integrating past chemical cleanings and predicting future τ_c states → takes into account the chemical pH of the secondary fluid
- ▶ THYC [Petit, 1991] is based on a finite-volume numerical scheme for the two-phase conservation equations
- ▶ Puffer is an in-house chemical code allowing to compute the solubility of iron oxides as a function of pH → used in the deposit model
- ▶ DEPO [Prusek et al., 2013] is the deposit module, solving the transport and clogging equations with iterative finite-differences schemes methods
- ▶ The chaining of these three codes is made on different criteria, more details are found in [Jaber et al., 2024] → unitary call is ~ 5 h on HPC infrastructure

Design of experiments

- ▶ Some experts exhibited a number of uncertain variables in the clogging model \rightarrow prior work done in [Lefebvre et al., 2023]
- ▶ In the DEPO module model, variables $\mathbf{X} = (X_1, \dots, X_d) \in \mathbb{R}^d$, with $d = 7 \rightarrow$ how these parameters affect the long term τ_c prognosis uncertainty? \rightarrow sensitivity analysis - work done in [Jaber et al., 2024]
- ▶ Assume $\mathbf{X} \sim \mu = \mathcal{U}(I_1) \otimes \dots \otimes \mathcal{U}(I_d)$ with support intervals given by experts and code designers \rightarrow use Latin Hypercube Sampling to draw $n = 10^3$ points and build

$$\text{DoE}_{\text{LHS}}^{\text{TPD}}(\mathbf{X}) = \{(\mathbf{X}^{(i)}, g(\mathbf{X}^{(i)}))\}_{i=1}^n \quad (1)$$

- ▶ Output is a vector $g(\mathbf{X}) = (g(\mathbf{X}, t_1), \dots, g(\mathbf{X}, t_N))$ of reduced dimension $N \sim 10^2$

Uncertainty propagation numerical results

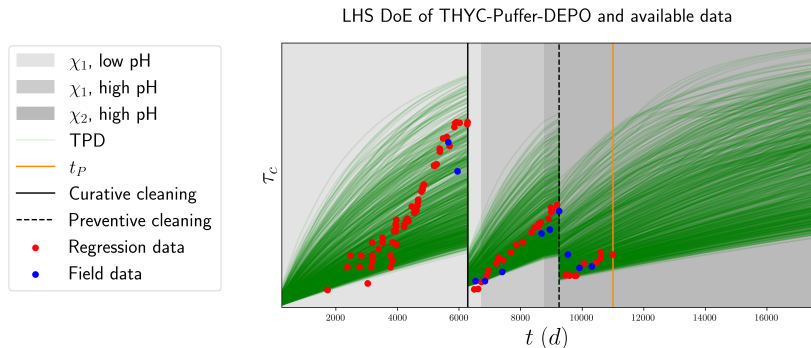


Figure: Illustration of output of $\text{DoE}_{\text{LHS}}^{\text{TPD}}(\mathbf{X})$ on a specific SG for a given simulation time, available field and regression data, the present time t_P is highlighted in orange

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Bayesian calibration methodology for RUL update

- ▶ Sensitivity analysis results highlight potential dependence on the output of $X_7 = \theta \rightarrow$ parameter related to the *vena contracta* phenomenon in the deposit model [Prusek et al., 2013]
- ▶ **Idea:** use the available field & regression data to update the prior distribution of $\theta \rightarrow$ reduce the future prediction uncertainty

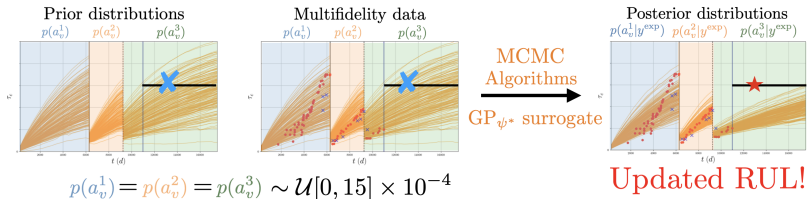


Figure: Bayesian calibration methodology for updating the RUL \rightarrow make use of Markov-Chain Monte-Carlo (MCMC) algorithm with optimized Gaussian process surrogate (GP) of the code. The multifidelity data comprises field data (FD) and regression data (RD)

Bayesian calibration formalism

- ▶ Three distributions of θ are calibrated for each period \rightarrow before *curative cleaning* (CC), between *curative cleaning and preventive cleaning* (CC-PC), and after *preventive cleaning* (PC) \rightarrow choice justified by the observed change in kinetics after a chemical cleaning
- ▶ Build, optimize & use a GP surrogate model \tilde{g}_{TPD} for fast sampling (since actual model calls are time-prohibitive) \rightarrow procedure based on $m = n + 1$ calibrations where n is the number of cleanings performed on a SG (in this example $m = 3$)
- ▶ Data between the k -th and $k + 1$ -th chemical cleaning:

$$\{\mathbf{y}_k^* = (y_{k,1}^*, \dots, y_{k,n_k}^*)\} \subset \{\mathbf{y}_1^*, \dots, \mathbf{y}_m^*\} \quad (2)$$

$\mathcal{J}_{*,k}$ are the respective time step indices, $n_{*,k} := |\mathcal{J}_{*,k}|$ with $* = \{\text{FD}, \text{RD}\}$

Bayesian calibration formalism

- ▶ Without model discrepancy, assume [Carmassi et al., 2019] for $k = 1, \dots, m$, with $* = \{\text{FD}, \text{RD}\}$:

$$\mathbf{y}_k^* = \mathcal{G}_k^*(\theta_k) + \boldsymbol{\eta}_k^*, \quad \boldsymbol{\eta}_k^* \sim \mathcal{N}(0, \sigma_*^2 I_{n_{*,k}}) \quad (3)$$

where \mathcal{G}_k^* applies the projection of the outputs of the surrogate model $\tilde{\mathcal{g}}_{\text{TPD}}$ onto time steps of the $*$ -th data between the k -th and $k + 1$ -th chemical cleaning

- ▶ Choice of priors for all k :
 - ▶ $\theta_k \sim \mathcal{U}[0, 15] \times 10^{-4}$
 - ▶ Jeffreys prior for $v := 1/\sigma_*^2$, $p(v) = 1/v$
 - ▶ θ_k and $\boldsymbol{\eta}$ are independent \rightarrow residuals give a Gaussian likelihood
- ▶ If all field data have the same standard deviation, then we can show that [Keller et al., 2022]:

$$p(\theta_k | \mathbf{y}_k^*) \propto \|\mathbf{y}_k^* - \mathcal{G}_k^*(\theta_k)\|^{-n_{*,k}} \quad (4)$$

Bayesian calibration formalism

- ▶ This posterior distribution can be generalized for q groups of multifidelity data $(\mathbf{y}^{\text{exp},1}, \dots, \mathbf{y}^{\text{exp},q})$ with different variances (in our case $q = 2$ since FD and RD have different variances) for $k = 1, \dots, m$:

$$p(\theta_k | \mathbf{y}_k^{\text{FD}}, \mathbf{y}_k^{\text{RD}}) \propto \|\mathbf{y}_k^{\text{FD}} - \mathcal{G}_k^{\text{FD}}(\theta_k)\|^{-n_{\text{FD},k}} \times \|\mathbf{y}_k^{\text{RD}} - \mathcal{G}_k^{\text{RD}}(\theta_k)\|^{-n_{\text{RD},k}}$$

- ▶ Weight associated with the * data type \rightarrow related to the number of data points $n_{\text{FD},k}, n_{\text{RD},k}$.
- ▶ MCMC algorithm of the Random-Walk Metropolis-Hastings type [Rubinstein and Kroese, 2011] in OpenTURNS Python library \rightarrow sampling from distributions $p(\theta_k | \mathbf{y}_k^{\text{FD}}, \mathbf{y}_k^{\text{RD}})$ + Gelman-Rubin convergence test for Markov chains

Numerical results

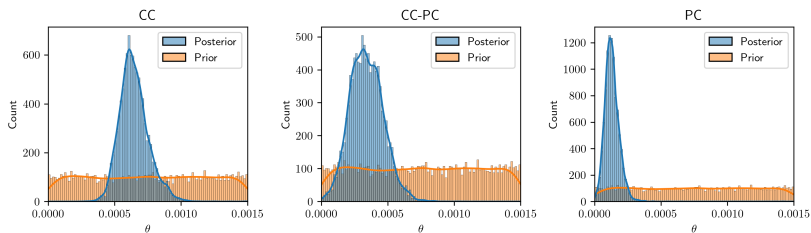


Figure: Prior and MCMC-sampled posterior distributions of the calibration parameter θ \rightarrow different modes after the different chemical cleaning actions \rightarrow confirms the prior operational knowledge and informs the physical model \rightarrow **hybrid approach!**

Updated uncertainty propagation

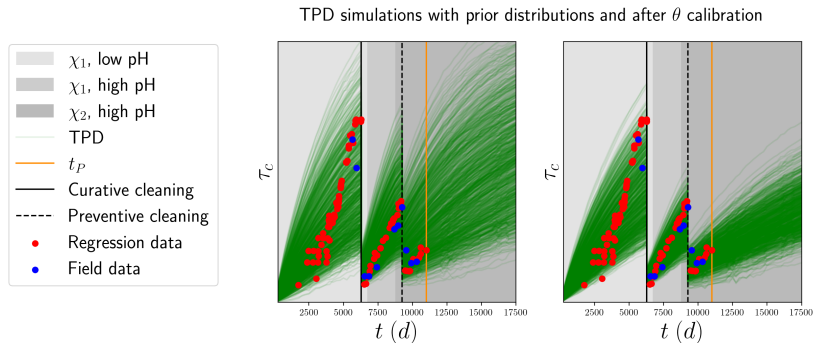


Figure: Uncertainty propagation with regular $\mathcal{U}(I_1) \otimes \dots \otimes \mathcal{U}(I_d)$ vs. updated posterior $\mathcal{U}(I_1) \otimes \dots \otimes \mathcal{U}(I_{d-1}) \otimes p(\theta | \mathbf{y}^{\text{RD}}, \mathbf{y}^{\text{FD}}) \rightarrow$ dispersion next to t_P is highly reduced \rightarrow decision-making more robust!

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Summary

- ▶ Clogging of SGs in PWR is a degradation phenomenon requiring diagnosis and prognosis for chemical cleaning planning → complex phenomenon, hard to model
- ▶ Making use of available knowledge to help decision-making in uncertain field → UQ methodology + Bayesian calibration allow to give more robust predictions
- ▶ Build controllable predictive machine learning algorithms that could be pilotable → based on sensor time-series operational data placed on the SG and the PWR → *work in progress*
- ▶ Hybrid methodology could be generalized to other degradation phenomena to provide decision-making assistance for predictive maintenance

Thank you for your attention!
Any questions?

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Sensitivity analysis: HSIC

- ▶ Hilbert-Schmidt Independence Criterion (HSIC) [Gretton et al., 2005], kernel method → evaluates sensitivity of a single-input in a given-data context, no need for surrogate models
- ▶ Theoretical result for all $i \in \{1, \dots, d\}, k \in \{1, \dots, N\}$:

$$\text{HSIC}(X_i, g(\mathbf{X}, t_k)) = 0 \iff X_i \perp g(\mathbf{X}, t_k) \quad (5)$$

- ▶ The index disposes of U-stat and V-stat estimators + hypothesis testing with corresponding p -value → implemented in the **OpenTURNS**
- ▶ The normalized R_{HSIC}^2 index is better suited for interpretation:

$$R_{\text{HSIC}}^2(X_i, g(\mathbf{X}, t_k)) = \frac{\text{HSIC}(X_i, g(\mathbf{X}, t_k))}{\sqrt{(\text{HSIC}(X_i, X_i)\text{HSIC}(g(\mathbf{X}, t_k), g(\mathbf{X}, t_k)))}} \in [0, 1]$$

- ▶ Empirical evidence suggests show that R_{HSIC}^2 can be used confidently for variable ranking → HSIC-ANOVA decompositions also exist *but* only pathological cases create stark differences (see [Sarazin et al., 2023])

Prior HSIC results

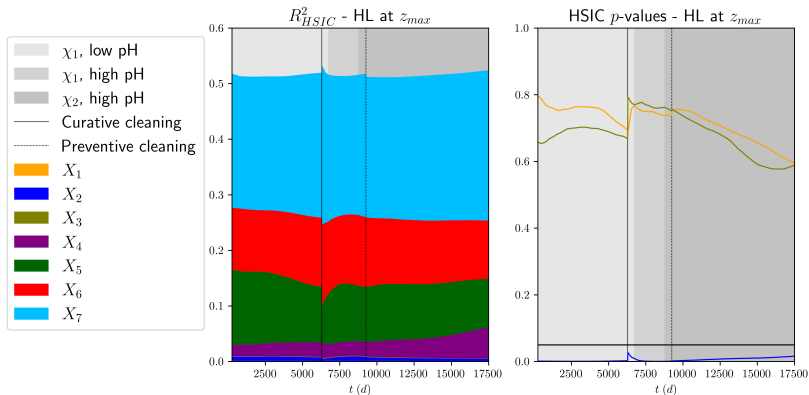


Figure: Normalized HSIC index time variation, ranking displays a potential strong dependence of X_7 on the output $\rightarrow X_7 = \theta$ is the calibration parameter of the DEPO model \rightarrow drives the τ_c kinetics

Posterior HSIC indices

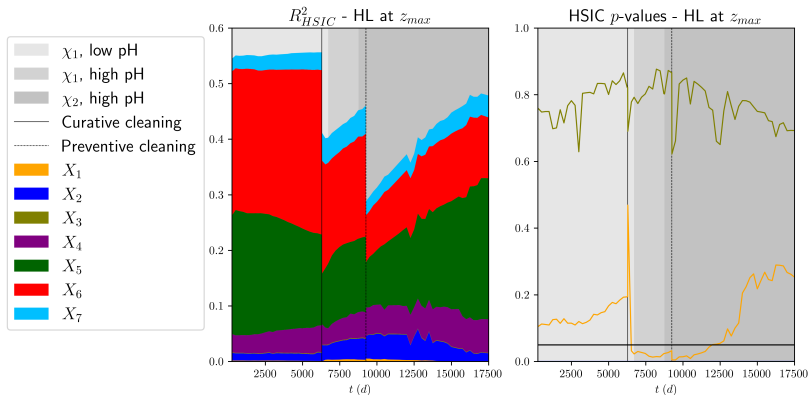


Figure: Normalized HSIC index time variation after calibration \rightarrow displays consequent influence reduction of the X_7 calibration component on the output

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